

Gravity Driven Membrane (GDM) disinfection

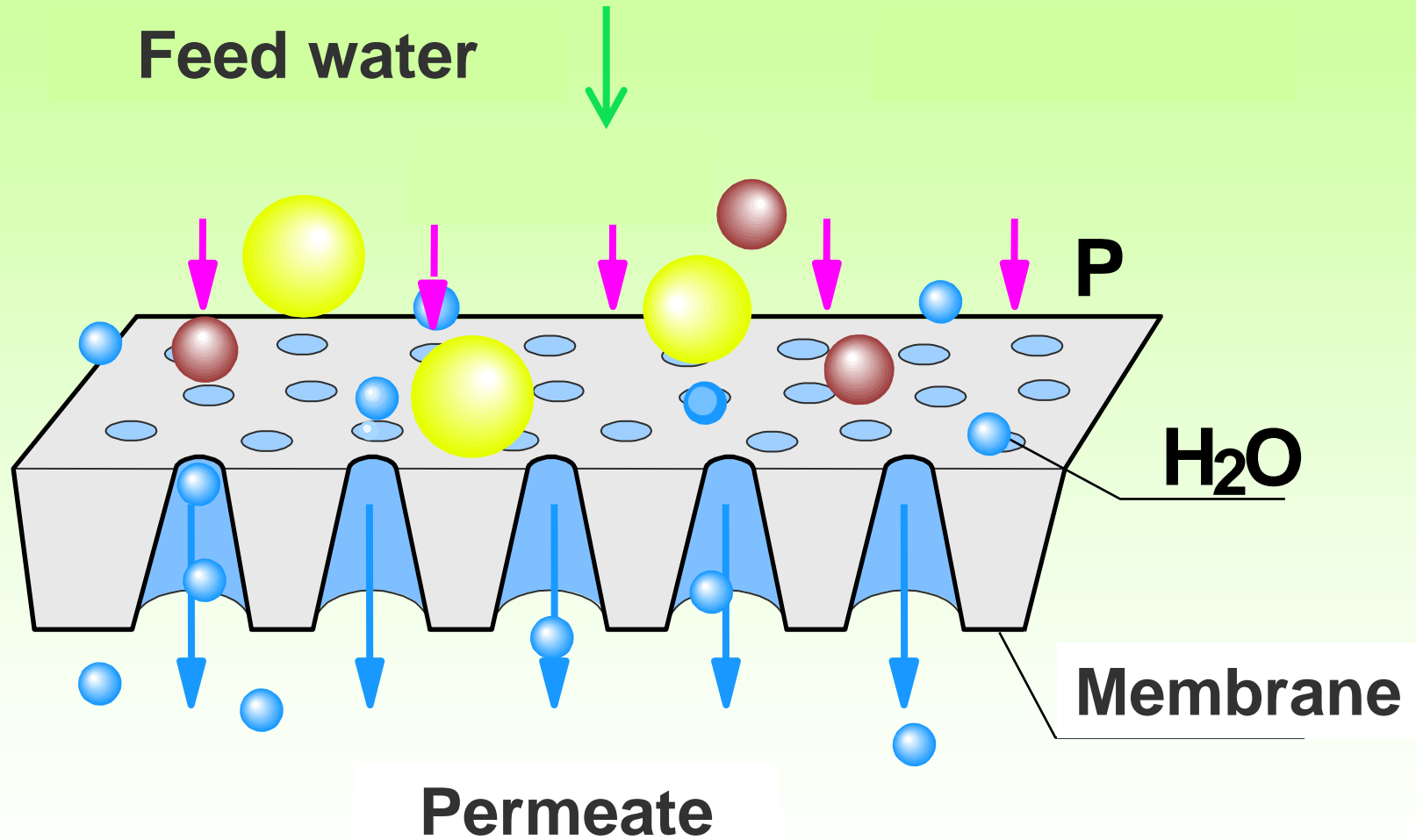
A novel household water treatment system

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Francis Kage, Regula Meierhofer, Selina Müller, Wouter Pronk*

UNC Water and Health Conference

October 4, 2011

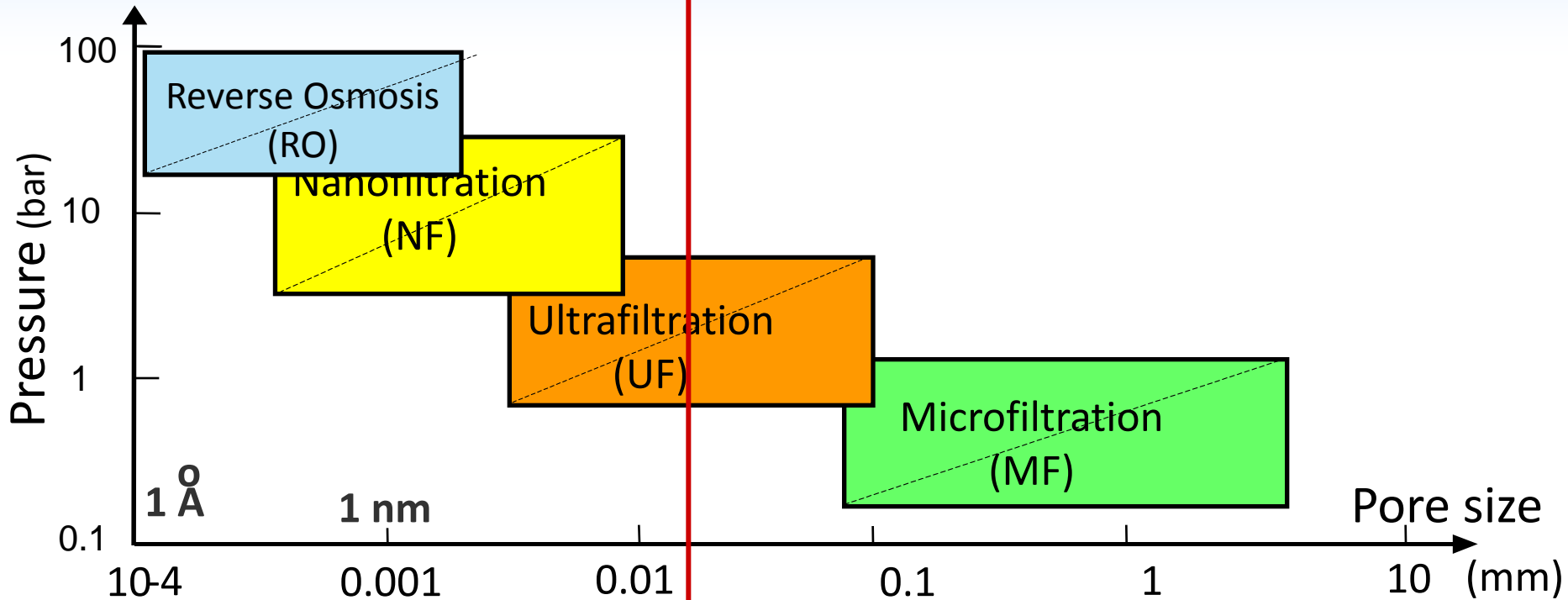
Principle of membrane filtration



Membrane filtration processes

Desalination

Disinfection



dissolved ions

hormones

humics
macromolecules

colloids

viruses

emulsions

bacteria

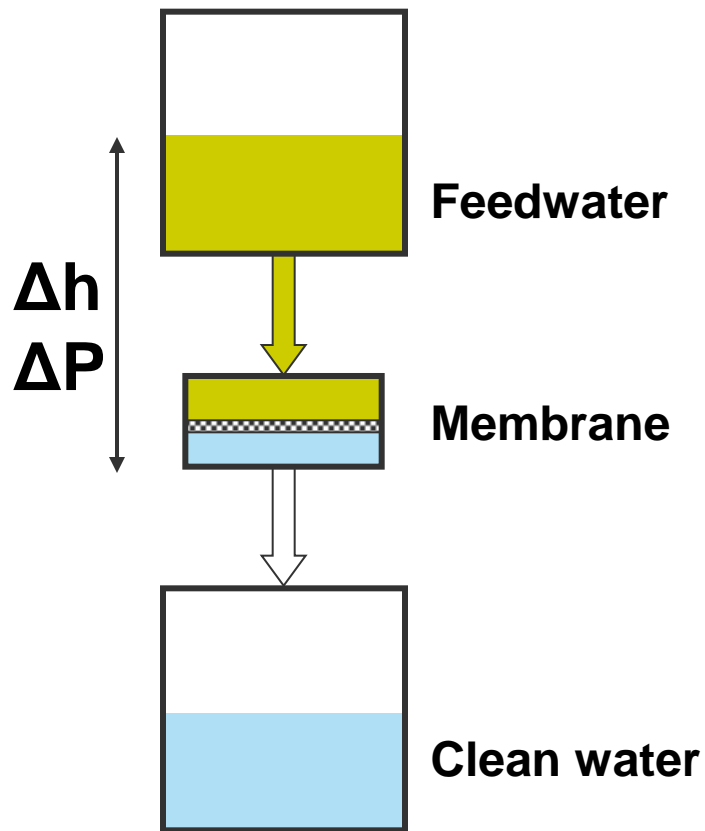
Ultrafiltration

Operation on any scale requires:

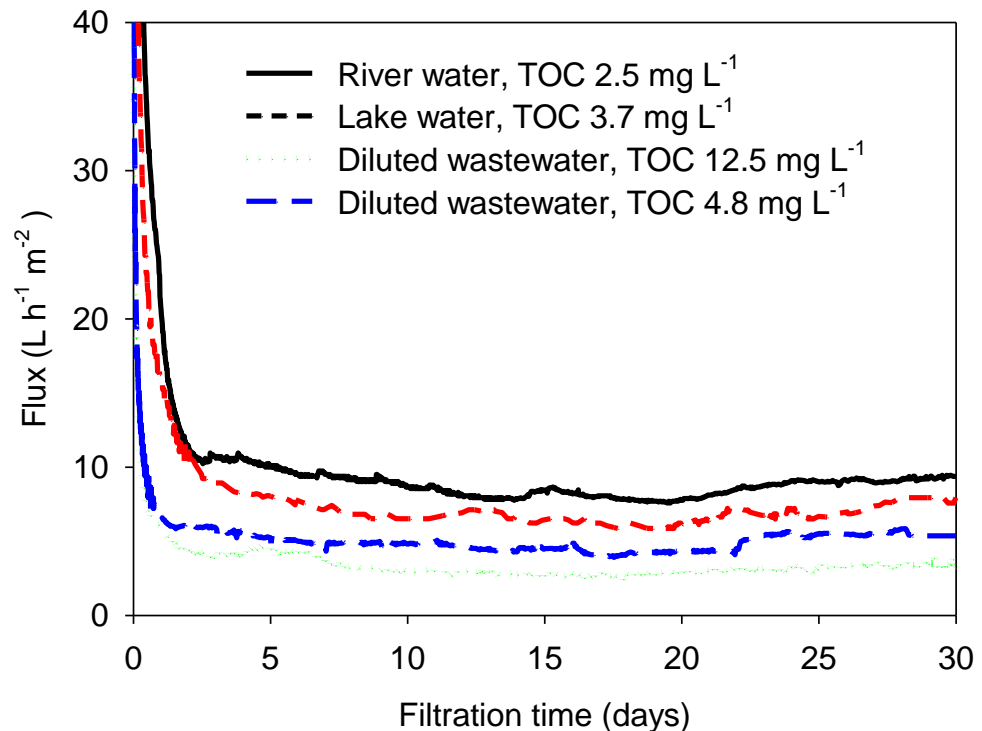
- ✓ Regular backflushing
- ✓ Disinfection
- ✓ Chemical cleaning
- ✓ Pre-treatment
- ✓ Pressure of 1-10 m water column



Gravity-driven Ultrafiltration



- **Dead-end, no cross-flow**
- **No backflush**
- **No chemical cleaning**



- **Stable flux: 4-10 L/h/m²**

Dried fouling layer

**Membrane
support layer**

**Membrane
separation layer**

Layer formed during 40 days of filtration of river water

100 μ m

EHT = 20.00 kV
WD = 35.0 mm

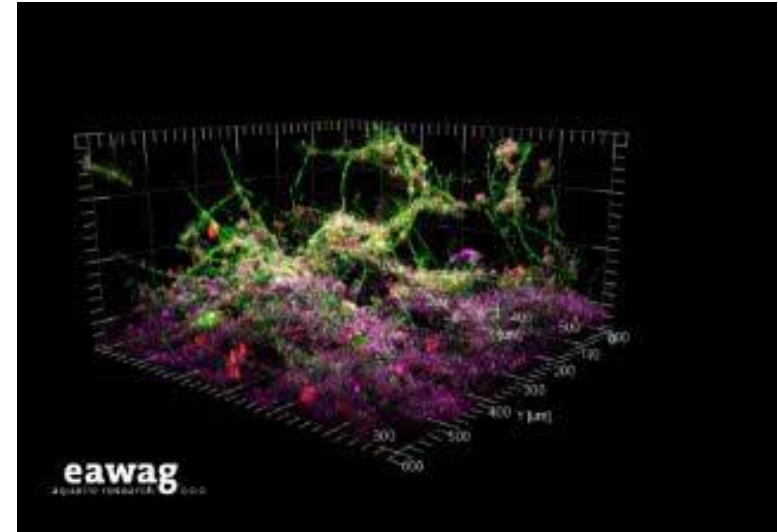
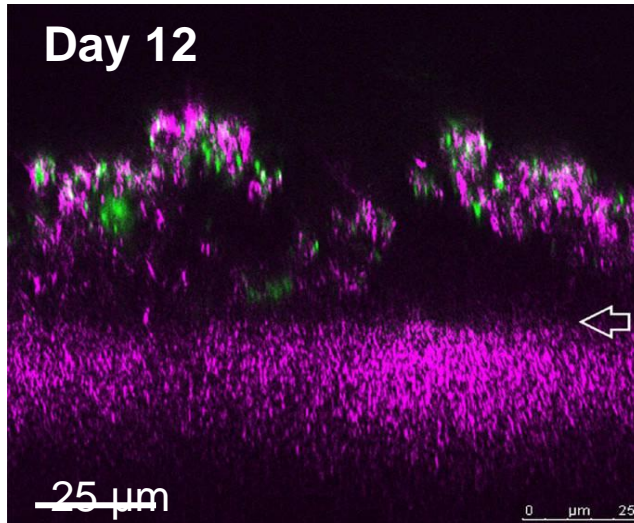
Mag = 400 X
Stage at T = 80.0 °

Signal A = SE2
File Name = 6044-CB-37 -1246.tif

Date : 19 Mar 2009
www.zmb.unizh.ch

ZMB

Fouling layer visualized by CLSM



- All bacterial cells (SYBR® Gold)
- Particles and the membrane (Reflection)

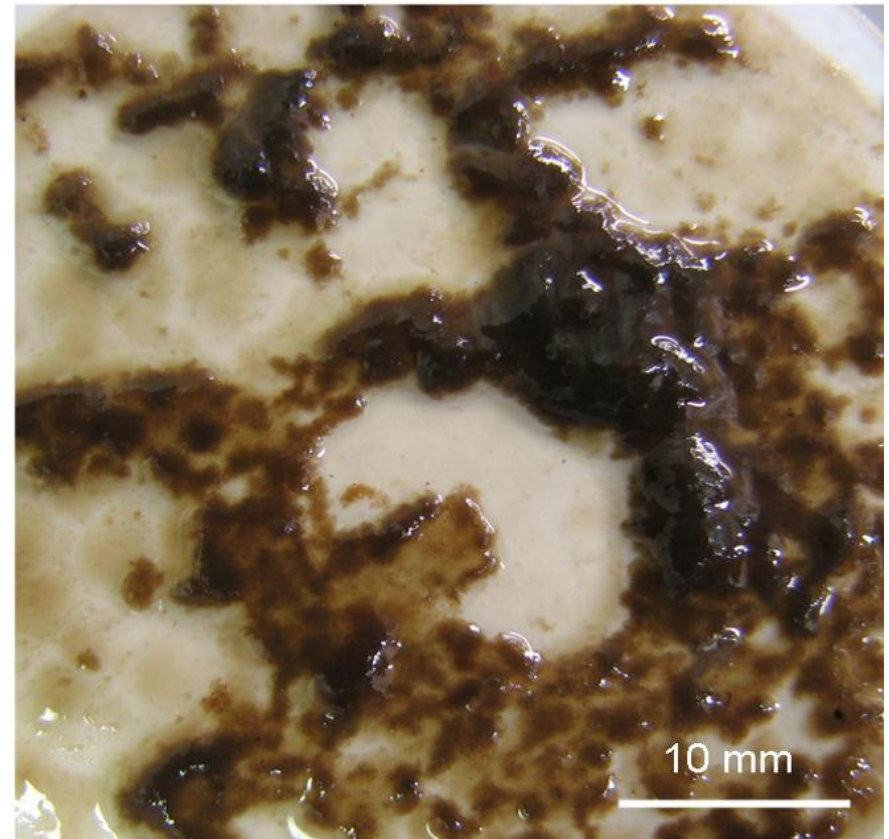
- Porous and heterogeneous fouling layer
→ reason of flux stabilization
- High presence of bacteria
→ importance of biological activity

Fouling layer structure on macro-scale

1 month, river water

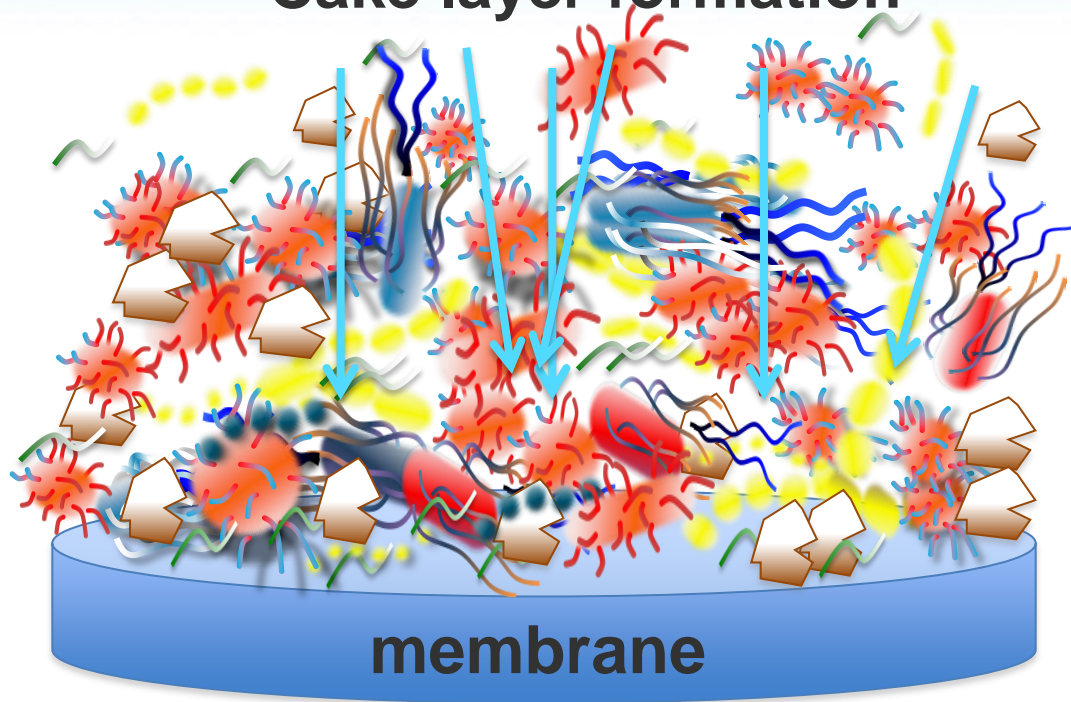


3 month, diluted wastewater



The changes of the fouling layer structure lead to the stabilization of flux

Cake layer formation



Structural changes within the fouling layer are caused by biological and physical processes in the layer

Lab studies, field trials, commercialization

Field evaluation

Kenya: 25 prototypes

Optimization and design

Virus removal efficiency

Membrane module optimization

Industrial design

Commercialization

Entrepreneurs, NGOs, membrane producers

Carbon credits

Long term planning

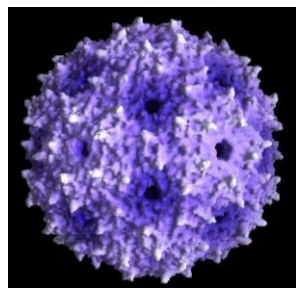
Development of long term strategies

Discussions with private sector

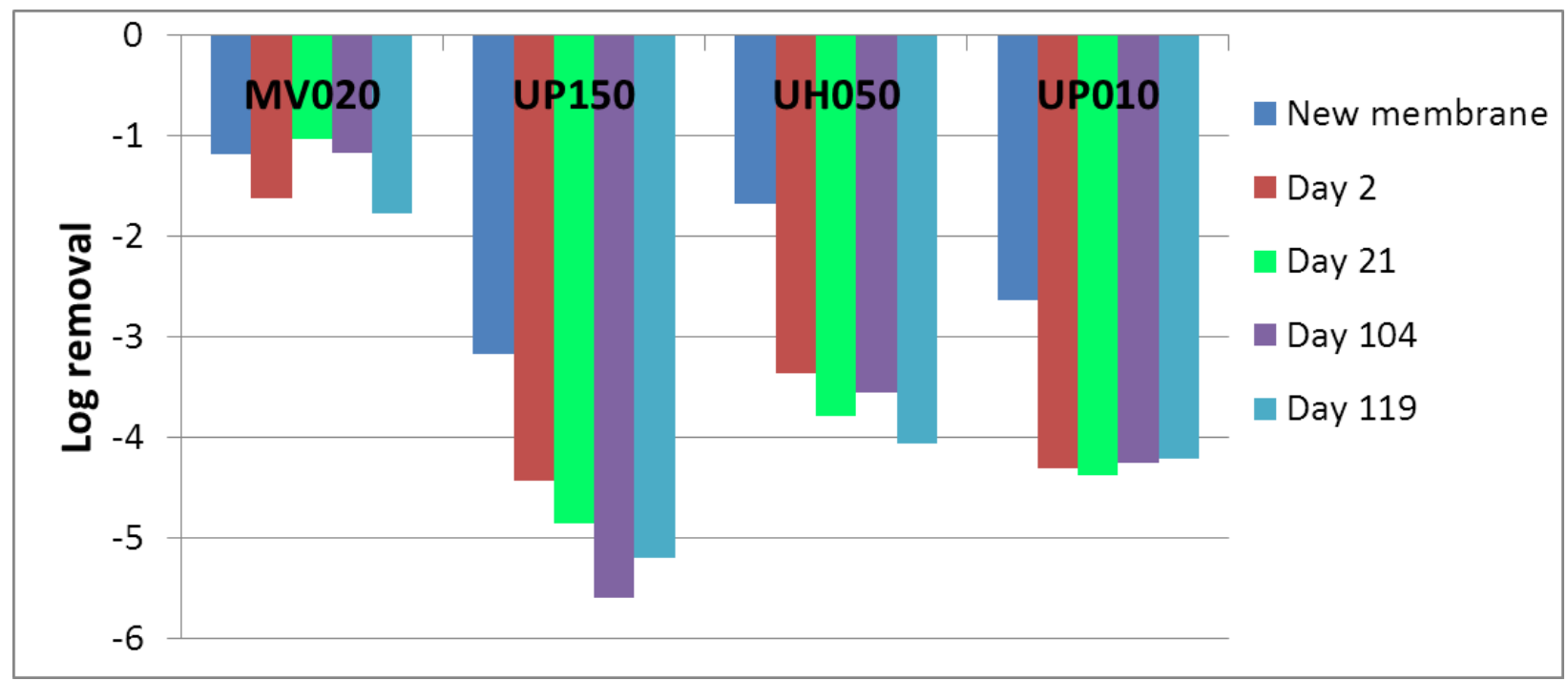
Private donor



Virus removal



Challenge tests: MS2 bacteriophage



GDM Field trials in Kenya

Alpha prototype GDM filter



Pre-filter (cloth)

UF membrane:

- Microdyn-Nadir
- 150 kDa cut-off (about 40nm pore size)
- 0.6 m² surface area (full)



Clean water tank, 10L



25 filters: diverse water sources

Kajiado (n=16)

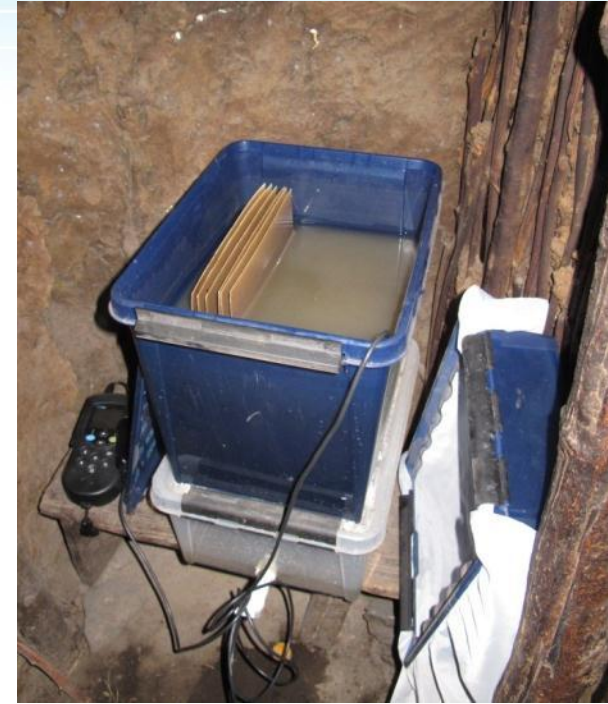
Pond water, borehole, open shallow wells
organic matter, turbidity, Fe

Thika (n=5)

Thika river
organic matter, turbidity

Nairobi (n=4)

Distribution network
chlorine



Monitoring

Frequency of use and flux

Submersible dataloggers

Water quality

Microbial: Nissui Compact Dry Plates, ATP

Conductivity, Oxygen, pH, Fe

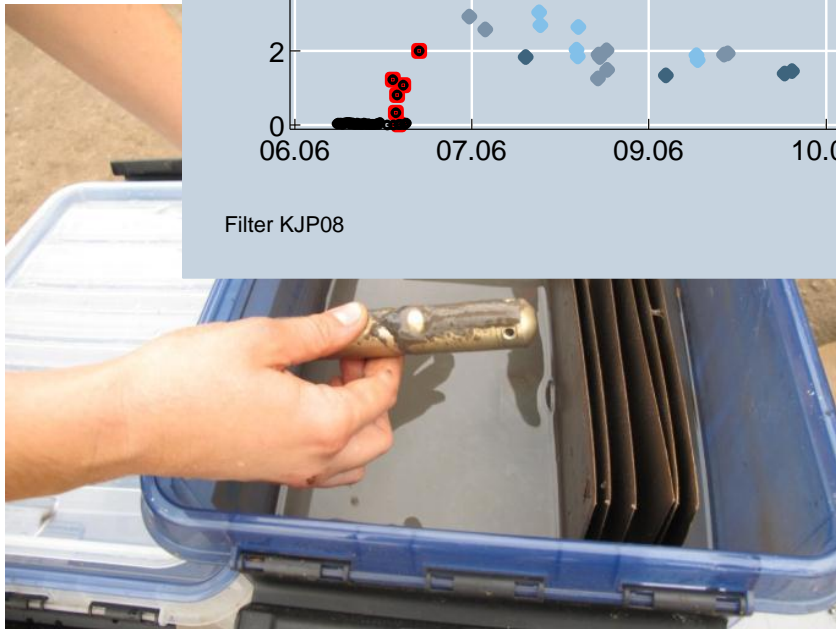
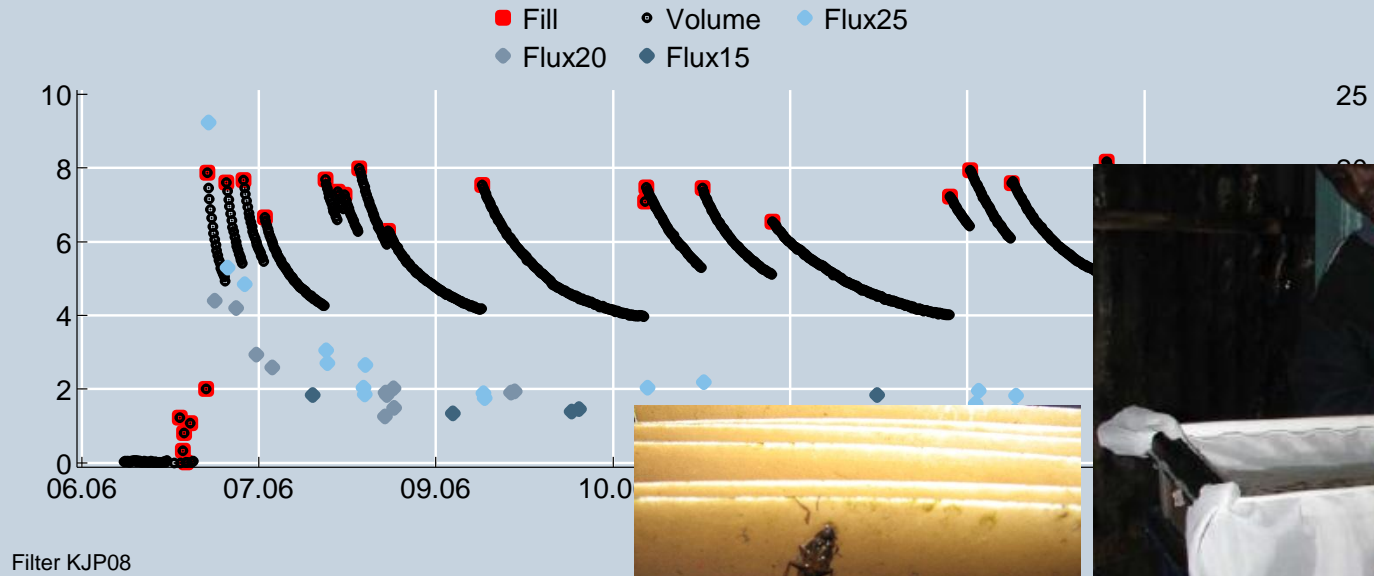
End-user perception

Observation, Household surveys



Frequency of use and flux

Filter use and performance



25

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Preliminary results (3 months)

- ✓ Good pathogen removal
 - ✓ Low *E. coli* inputs
- ✓ Stable flux in spite of thick fouling layer
- ✓ Regular use
 - ✓ 100% functioning
- ✓ Relatively high acceptance

- Re-contamination and/or re-growth
 - Total coliforms, ATP
 - Flux lower than in lab

- ➔ Design improvements



Next steps: September 2011- June 2012

Technology

- Temperature
- Microbial re-growth

Design

- User interface
- Membrane module

Field evaluation

- Monitoring
- Second generation of prototypes
- Re-growth/recontamination, viruses

Business models

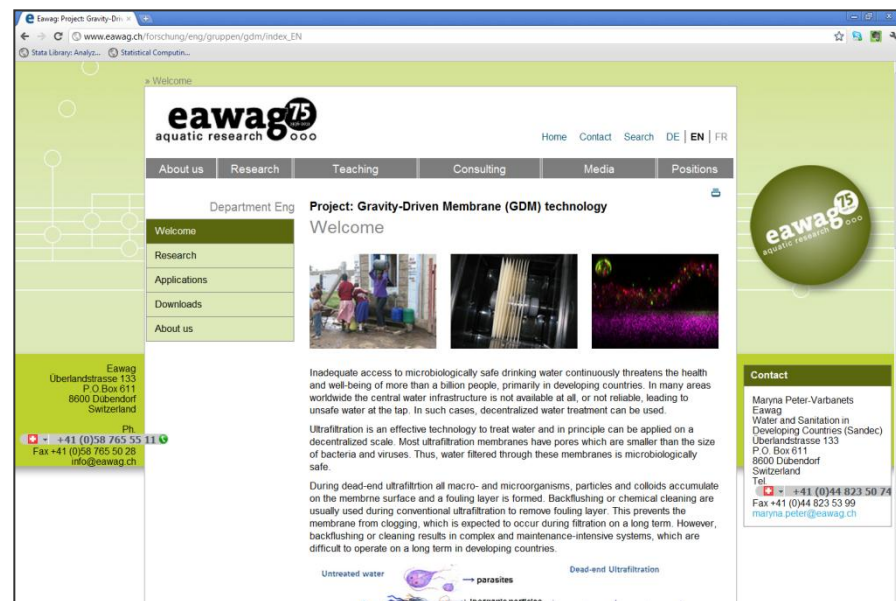
- Distribution channels, supply chain
- Social Marketing
- Pricing and subsidy (including carbon credits)
- Business plan for Foundation

Foundation

- Private donor
- Research support
- Product commercialization, investment

Many thanks to

- Kenya Water for Health Organization
- Workshop staff of Kenya Water Institute
- Public Health Officer of Kajiado
- The people of Kajiado, Thika, and Woodley



Further information

www.eawag.ch/membranefilter